

**ME 24-221**  
**Thermodynamics I**

Solution to Assignment No: 7  
Due Date: 27 October 2000  
Fall 2000  
Instructor: J.Murthy

Pb# 6.41

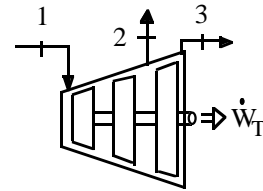
Supply state 1: 20 kg/s at 10 MPa, 500C

Process steam 2: 5 kg/s, 0.5 MPa, 155 C,

Exit state 3: 20 kPa,  $x = 0.9$

Table B.1:  $h_1 = 3373.7$ ,  $h_2 = 2755.9$ ,

$$h_3 = 251.4 + 0.9 \times 2358.3 = 2373.9$$



Energy Eq.:  $\dot{Q}_{CV} + \dot{m}_1 h_1 = \dot{m}_2 h_2 + \dot{m}_3 h_3 + \dot{W}_{CV}$  ;

$$\dot{W}_{CV} = 20 \times 3373.7 - 5 \times 2755.9 - 15 \times 2373.9 = \mathbf{18.084 \text{ MW}}$$

Pb# 6.46

$$h_1 = 763.5 = 604.74 + x \times 2133.8 \Rightarrow x = 0.07439 = \dot{m}_2 / \dot{m}_1$$

Table B.1.2:  $h_2 = 2738.6$ ;  $h_3 = 191.83 + 0.9 \times 2392.8 = 2345.4$

$$\dot{W} = \dot{m}_2 (h_2 - h_3) \quad \dot{m}_2 = \frac{1000}{2738.6 - 2345.4} = 2.543$$

$$\Rightarrow \dot{m}_1 = 34.19 \text{ kg/s} = \mathbf{123075 \text{ kg/h}}$$

Pb# 6.47

a) CV: Compressor

$$\begin{aligned} \dot{Q}_{COMP} &= \dot{m}(h_1 - h_e) + \dot{W}_{COMP} \\ &= 0.05(260.023 - 191.009) - 4.0 = \mathbf{-0.549 \text{ kW}} \end{aligned}$$

b) CV: Condenser

$$\dot{Q}_{COND} = \dot{m}(h_3 - h_2) = 0.05(79.647 - 252.720) = \mathbf{-8.654 \text{ kW}}$$

c) CV: Evaporator  $h_4 = h_3 = 79.647$  (from valve)

$$\dot{Q}_{EVAP} = \dot{m}(h_5 - h_4) = 0.05(187.583 - 79.647) = \mathbf{5.397 \text{ kW}}$$

Pb# 6.48

$$1 : 1 \text{ MPa}, 200^\circ\text{C}, m_1 = P_1 V_1 / RT_1 = 1000 \times 0.1 / (0.287 \times 473.1) = 0.736 \text{ kg}$$

$$2 : 100 \text{ kPa}, 50^\circ\text{C}, m_2 = P_2 V_2 / RT_2 = 100 \times 0.1 / (0.287 \times 323.1) = 0.1078 \text{ kg}$$

$$m_{\text{ex}} = m_1 - m_2 = 0.628 \text{ kg}, \quad m_2 u_2 - m_1 u_1 = -m_{\text{ex}} h_{\text{ex}} + {}_1 Q_2$$

$$\text{Table A.7: } u_1 = 340.0 \text{ kJ/kg}, \quad u_2 = 231.0 \text{ kJ/kg},$$

$$h_{\text{e ave}} = (h_1 + h_2) / 2 = (475.8 + 323.75) / 2 = 399.8 \text{ kJ/kg}$$

$${}_1 Q_2 = 0.1078 \times 231.0 - 0.736 \times 340.0 + 0.628 \times 399.8 = \mathbf{+25.7 \text{ kJ}}$$

Pb# 6.52

C.V. turbine & tank  $\Rightarrow$  USUF

$$\text{Conservation of mass: } m_1 = m_2 \Rightarrow m$$

$$\text{Energy Eq: } m_i h_i = m_2 u_2 + W_{\text{CV}}; \quad W_{\text{CV}} = m(h_i - u_2)$$

$$\text{Table B.6 : } i : P_i = 0.5 \text{ MPa}, T_i = 300\text{K}, \text{ Nitrogen; } h_i = 310.276 \text{ kJ/kg}$$

$$2: P_2 = 0.5 \text{ MPa}, T_2 = 250 \text{ K}, u_2 = h_2 - P_2 v_2$$

$$u_2 = 257.799 - 500(0.14782) = 180.89 \text{ kJ/kg}$$

$$m_2 = V / v_2 = 50 / 0.14782 = 338.25 \text{ kg}$$

$$W_{\text{CV}} = 338.25(310.276 - 180.89) = 43764.8 \text{ kJ} = \mathbf{43.765 \text{ MJ}}$$

Pb# 6.58

$$\text{1st law: } m_i h_i = (m_2 u_2 - m_1 u_1)_{\text{AIR}} + m_{\text{ST}}(u_2 - u_1)_{\text{ST}}$$

$$m_1 \text{ AIR} = \frac{P_1 V}{RT_1} = \frac{500 \times 1}{0.287 \times 293.2} = 5.94 \text{ kg}$$

$$m_2 \text{ AIR} = \frac{P_2 V}{RT_2} = \frac{1500 \times 1}{0.287 \times T_2}$$

$$m_i = (m_2 - m_1)_{\text{AIR}} = (5226.5 / T_2) - 5.94$$

$$[(5226.5 / T_2) - 5.94] \times 1.004 \times 293.15 = \frac{5226.5}{T_2} \times 0.717 \times T_2$$

$$- 5.94 \times 0.717 \times 293.15 + 40 \times 0.48 (T_2 - 293.15)$$

$$\text{Solving, } T_2 = 321.3 \text{ K} = \mathbf{48.1^\circ\text{C}}$$