

PROGRESS OF NANOFILTRATION MEMBRANES

**1st Korea-US Nano Forum
2003. 10. 14**

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OVERVIEW

- **Introduction of Nanofiltration(NF)**
- **NF Application**
 - in Aqueous system
 - in Non-aqueous system
- **NF Membranes developed in KRRICT**
 - Fouling resistant membrane
 - Solvent resistant membranes
- **Summary**

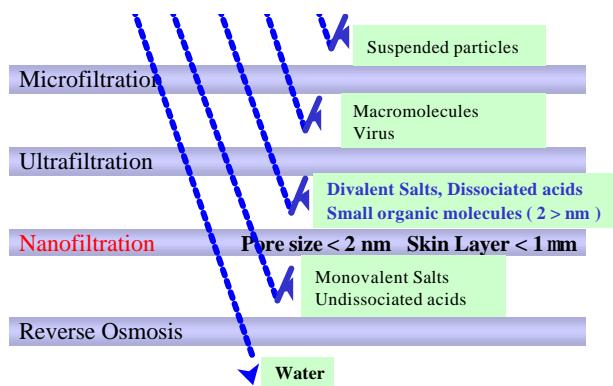
Application range of various membrane process

Particle size μm nm	atomic/ ionic range 0.001 1.0	low molecu- lar range 0.01 1.0	high molecu- lar range 0.1 10	micro particle range 100	macro particle range 1.0 1000 10,000
Molecular weight	100 200	1000	100,000	500,000	
Solute	aqueous salt metal ion sugar		colloidal silica virus proteins microsolutess		yeast cells bacteria
Membrane separation process	electrodialysis diffusion dialysis reverse osmosis gas separation permeation	nanofiltration dialysis		ultrafiltration	microfiltration

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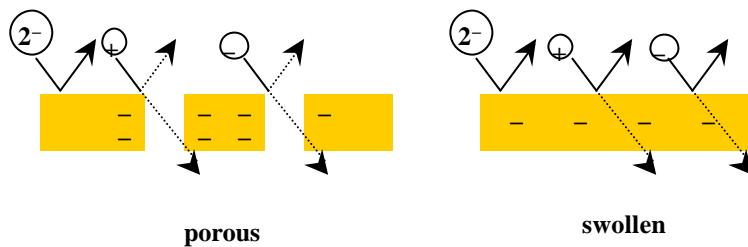
NANOFILTRATION (NF) MEMBRANES

- Membranes whose performance is in **between those of UF and RO** (MWCO: 200-1000 g/mole)
- Good rejection of multivalent ions or organic materials with low molecular weight
- Low Operating pressure



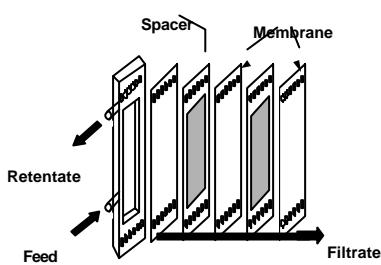
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Schematic drawing of separation of ions by negative nanofiltration membranes

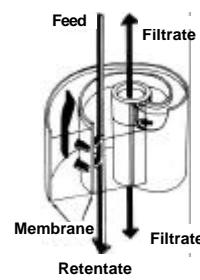


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Membrane modules



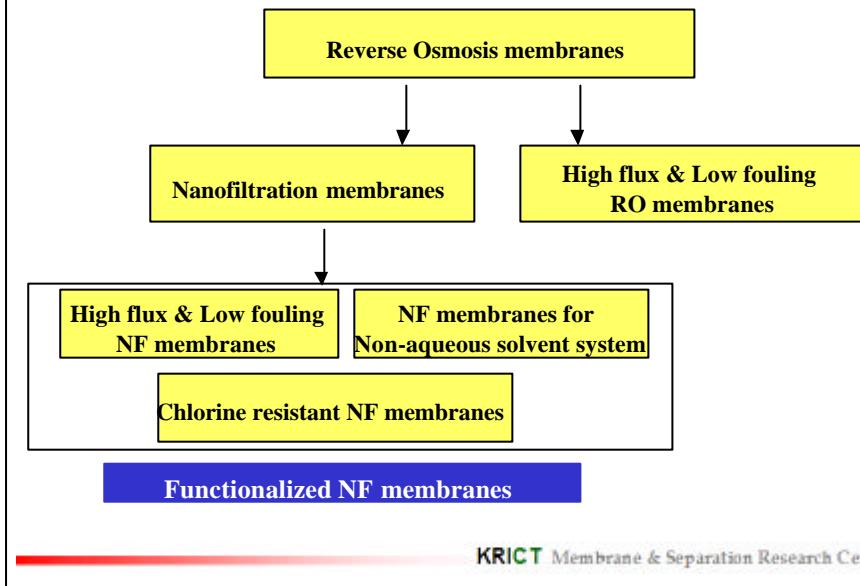
(a) Plate type module



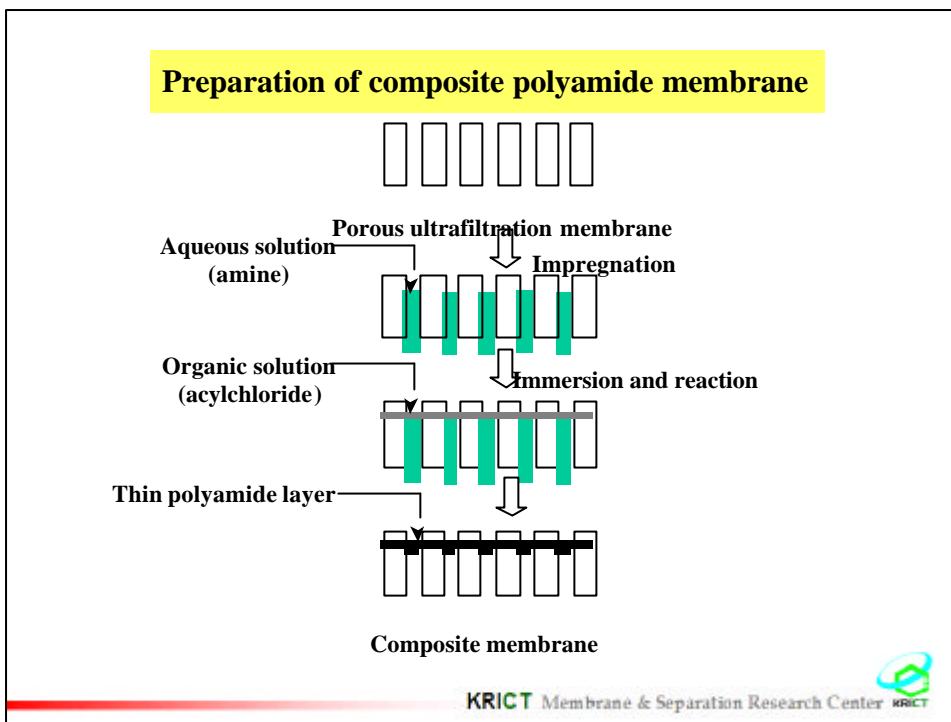
(b) Spiral-wound type module

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Progress in Nanofiltration Membranes

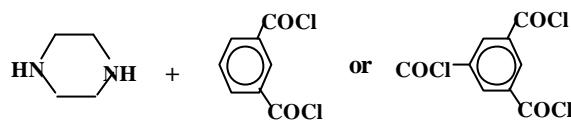


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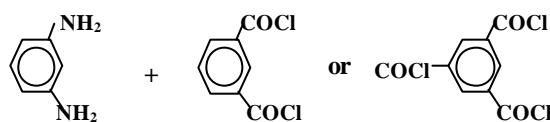
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Polypiperazineamide ; NF membrane



NF-40(FilmTec); NTR-7250, NTR-729(Nitto Denko); UTC-20/50/60(Toray)

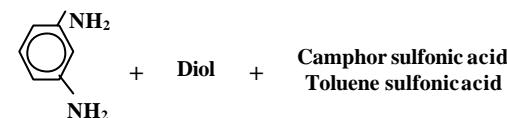
Polyamide; RO & NF membrane



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High flux RO & NF membranes



Aqueous solution



Significant flux enhancement due to the surface roughness increase

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Low fouling RO & NF membranes

High flux RO & NF membrane



Coating neutral polymers or inorganic material

Fouling resistance due to the surface charge blocking

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Solvent resistant NF membranes

Cross-linked PAN UF membrane



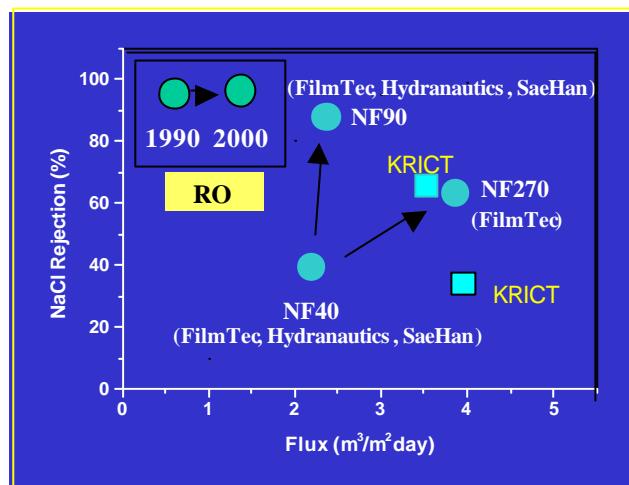
Coating silicone

Kyriat weizmann; MPF series

Solvent resistant against almost all solvents; Large pore (400 – 700Da)

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Progress of NF membranes

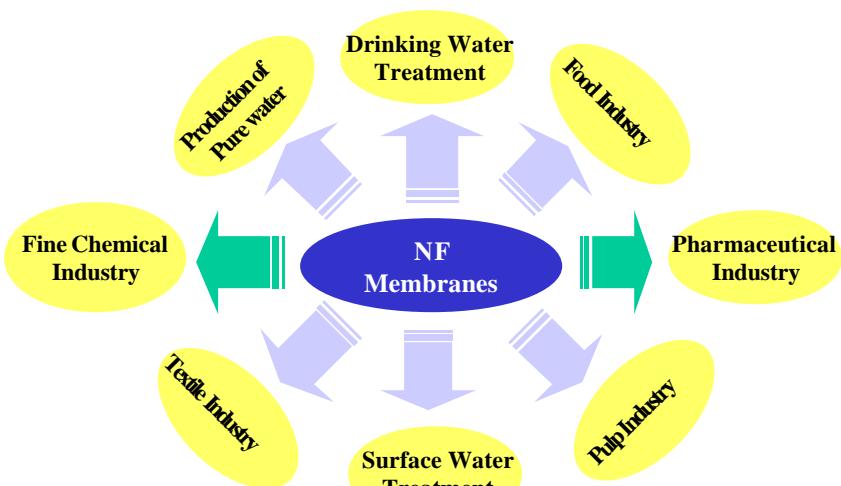


225 psi; 2000 ppm NaCl



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EXTENSION OF NF APPLICATION



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NF for Aqueous System

A. Drinking and Process Water Treatment

- Water softening and Pure water production
- Potable Water Production
- Surface and Ground water Treatment

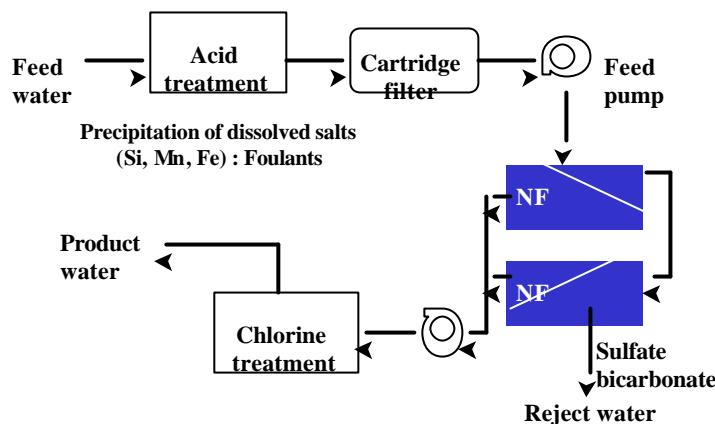
B. Wastewater Treatment

- Oily Wastewater
- Removal of Dye, VOC and Heavy Metals
- Chemical plant Wastewater
- Textile and Pulp Wastewater

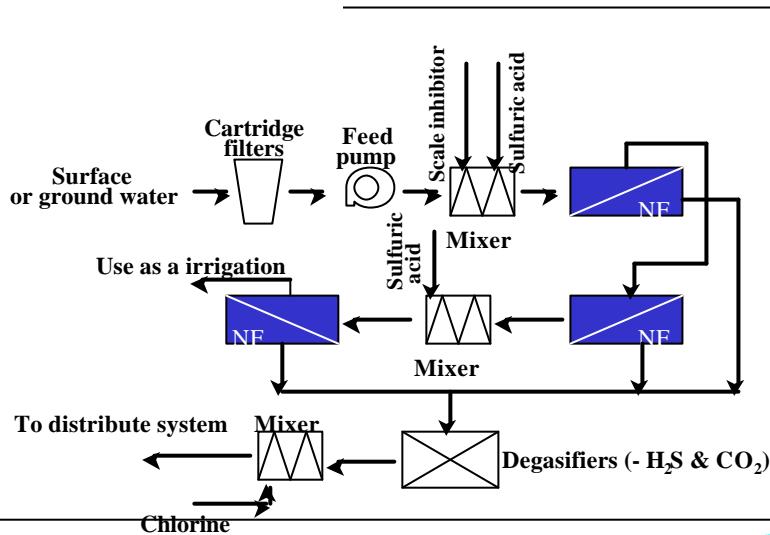
C. Food Industry

- Desalting of cheese whey and sea food processing
- Concentration of fruit juice
- Yeast Production

Water Softening



Potable Water Production



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NF for Non-aqueous System

A. Fine Chemical Industry

- The separation of organometallic catalysts
- The separation of small molecular weight organics (300-1000Da) or residual reactants produced from the synthesis in an organic solvent-based systems

B. Pharmaceutical Industry

- The separation of pharmaceuticals (300-1000Da) synthesized in a variety of organic solvents via a multi-step synthetic route

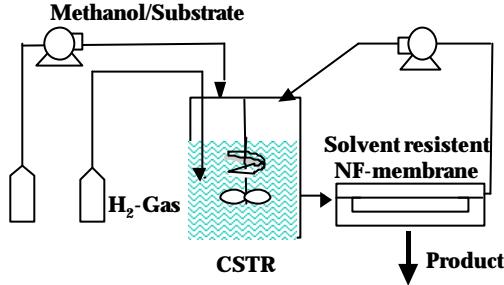
C. Vegetable Oil Industry

- The recovery of solvents used in the extraction of edible oil processing
- The concentration of edible oil
- The separation of denatured oil (fatty acid)

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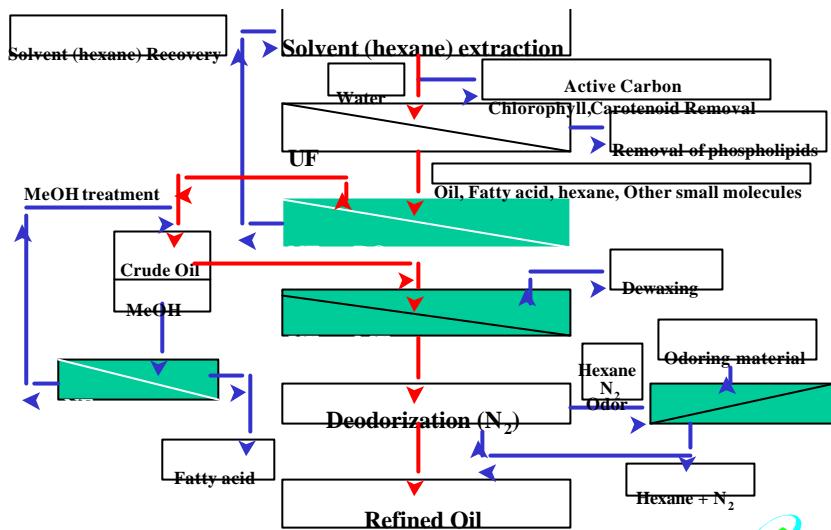
NF Membranes for Catalytic Reactor



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Membrane method for vegetable oil purification



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NF membranes studied in KRICT

1. Polyamide NF membranes (interfacial polymerization)

NF-90 : > 90% rejection of NaCl; underground water treatment

NF-70 : > 70% ; underground water treatment

NF-40 : > 40% ; surface water treatment

NF-20 : > 20% ; surface water treatment

Development trend : High flux and low fouling

2. Organic solvent-resistant NF membranes

Low swelling and high flux in organic solution

High separation of small molecular solute in organic solution

3. PVA & Integrally skinned NF membranes

Low fouling and chlorine resistant

Fouling-Resistant NF Membrane

• Fouling

A. Foulants

- Humic acid
- Colloids
- Surfactants
- Proteins
- Mineral salts
- Silica

B. Problems

- Increasing operation and maintenance costs
- Deteriorating membrane performance
- Shortening membrane

C. Properties influencing fouling

- Surface structure (roughness, pore size)
- Electrokinetic characteristics (ξ -potential)
- Chemical property (hydrophobic-hydrophilic interaction)

PVA-coated polyamide composite membrane

– Polyamides

Piperazine & m-phenylene diamine
Trimesoyl chloride

– Poly(vinyl alcohol)

Poly(vinyl alcohol) 0.05 wt%
Glutaraldehyde

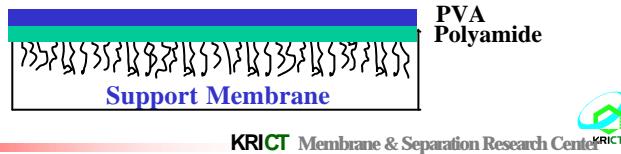
– Interfacial & Dip coating Method

– Support membrane

Polysulfone MWCO 50kDa

– Other NF membranes

NF 70
NF 70/PVA



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Change of membrane performance by PVA coating

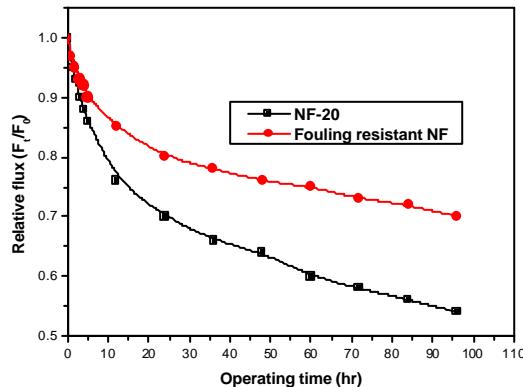
	PWF (m ³ /m ² day)	Rejection rate (%)	
		PEG 200	NaCl
PA	2.9	60	8
PA/PVA (1)	2.6	72	13
NF-70	1.7	81	75
NF-70/PVA (3)	1.4	88	83

25 °C; 200 psi

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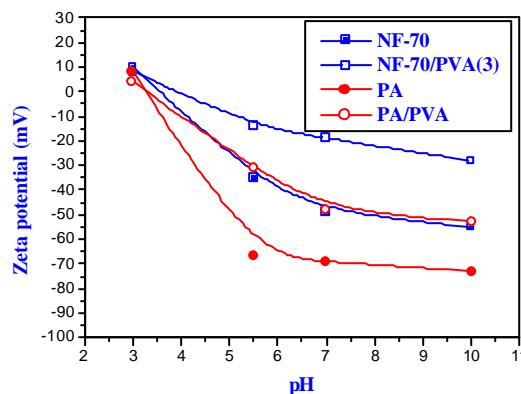
Neutral polymer- or nano particle-coated polyamide composite membrane

– Surface water treatment after microfiltration



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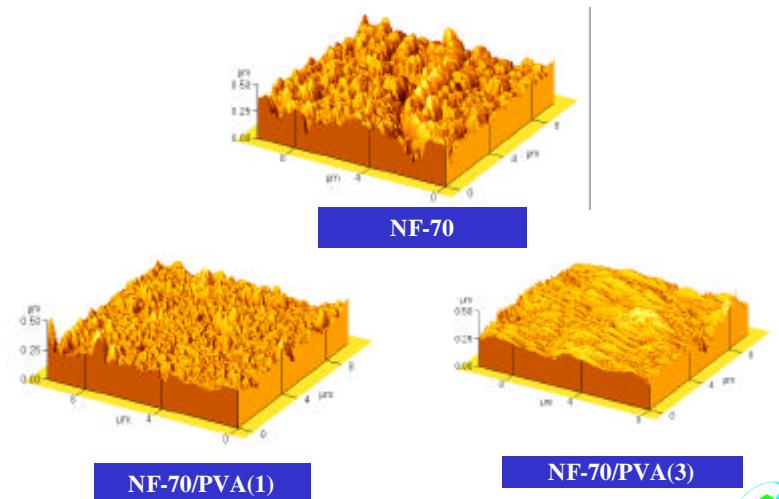
ζ -potential of PVA-coated NF membranes



Electro-phoretic method; pH 7.0; 0.01M NaCl

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AFM images of NF-70 & PVA/NF-70 membranes

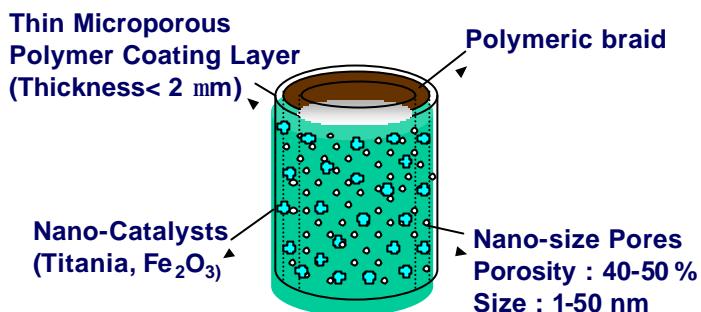


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Nano catalysts coated NF membranes

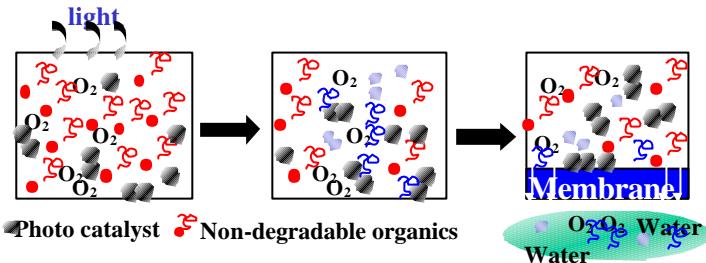
Integral multifunctional antifouling nano-complex- membranes
that would be efficient for the treatment of the waste-water
through nano-catalytic-reaction and separation



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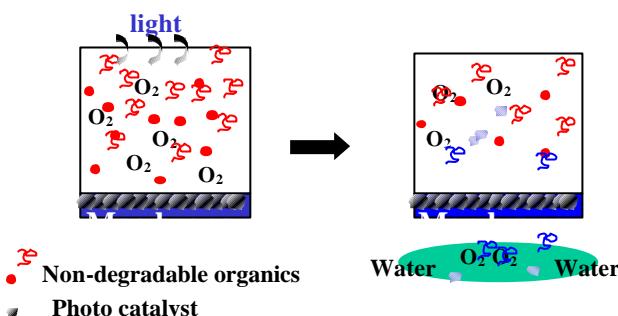
NF membrane -coupled Photo Catalyst Reactor



- Easy to recover the catalysts
- Need low-fouling NF membrane

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Nano catalysts-coated NF membrane reactor



- No need to recover the catalysts
- Low fouling by catalytic degradation of organics

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Solvent Resistant NF Membranes

Commercial NF membrane for non-aqueous system

MPF series (Kyriat Weizmann): MWCOs of 700 and 400Da
made with silicone

Advantage: high flux to organic solvent

Disadvantage: difficult to reduce pore size

Objectives of the present work

- Develop various types of NF membranes which is stable in organic solvents
- Investigate the possibility to separate fatty acid in methanol and acetone solution



Silicon Contained Polyamide NF Membranes

— Polyamides

Piperazine & m-phenylene diamine
Trimesoyl chloride

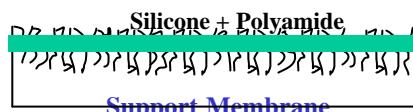
— Silicones

Polydimethylsiloxane (prepolymer A & cross-linker B)

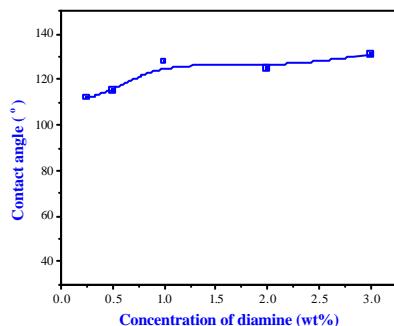
— Interfacial & Dip coating Method

— Support membrane

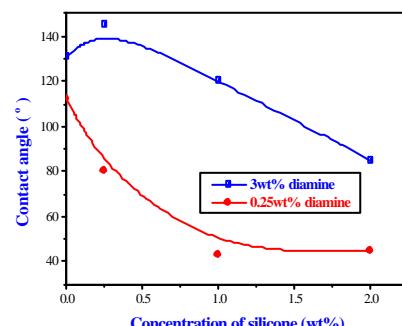
Phase inversion
PAN/NMP (15/85 wt%)
Coagulated in water



Contact angle of polyamide and silicone-contained polyamide NF membranes



Polyamide



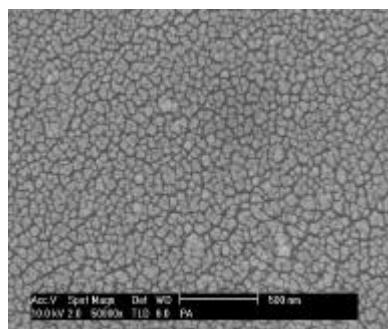
Silicone-based polyamide

Advanced angle of droplet formed by CCl₄ in water

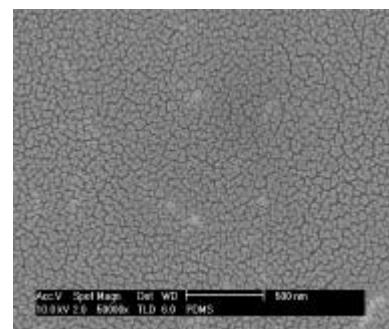
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SEM photographs of membrane surfaces



Polyamide

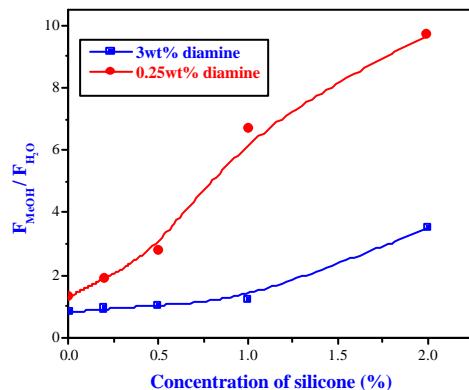


Silicone-based Polyamide

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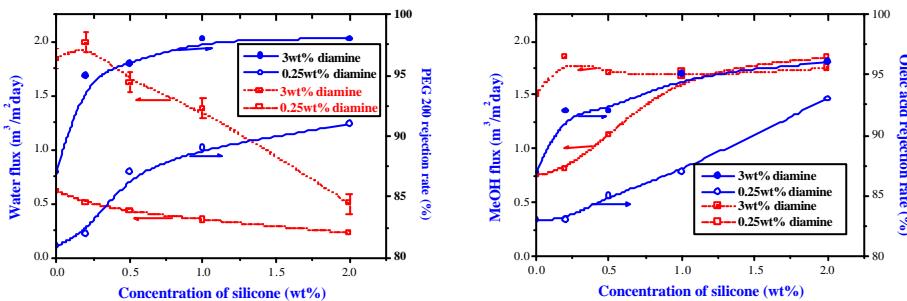


Flux ratio of MeOH to water of polyamide membrane



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Performance of silicone-contained PA NF membranes in aqueous and MeOH solution



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Concentrations of Diamines, 0.25 wt%

Silicone Conc. (wt%)	Solvent flux (TMD)						
	H ₂ O	MeOH	EtOH	IPA	acetone	MEK	Hexane
0	0.54	0.68	0.41	0.11	1.09	0.20	-
0.2	0.44	1.09	0.56	0.39	1.62	0.36	0.25
0.5	0.31	1.44	0.85	0.44	2.03	0.68	1.12
1.0	0.12	1.85	1.09	0.79	2.41	1.82	2.85
2.0	0.09	1.75	1.29	0.88	2.58	1.85	2.89

25 °C; 200 psi



SUMMARY

- Nanofiltration (NF) is rapidly growing in liquid phase separation for the removal of natural organic matter(NOM), multivalent salts, dyes, and small organic molecules.
- NF membranes with high flux, solvent resistance, and low fouling have been developed for the extension NF application range
- Membrane fouling is influenced by the membrane surface properties, such as surface roughness, charge and hydrophobic-hydrophilic properties and the PA membranes coated with a thin PVA layer or nano particles show very good fouling resistance
- For a non-aqueous NF system, solvent resistance of the membrane materials, and solvent fluxes are key issues. NF membranes prepared by blending of polyamide and silicone polymer show high solvent flux and high rejection to small organic molecules.