

**ME 24-221**  
**THERMODYNAMICS I**

Solution to First Mid-Term Exam  
October 5, 2000  
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Problem 1: Given: Closed rigid tank containing water

Initial state 1: water at critical point

Final state 2:  $T_2 = 100\text{ }^\circ\text{C}$

To find: Final quality

Solution: Critical constants for water are,  $T_c = 374.15\text{ }^\circ\text{C}$ ,

$$P_c = 22.12\text{ kPa,}$$

$$V_c = 0.00315\text{ m}^3/\text{kg}$$

Since it is a closed rigid tank the volume and mass are constant. Hence the specific volume  $v_c$ , is constant throughout the process.

At  $T_2 = 100\text{ }^\circ\text{C}$ ,  $v = v_c$ ,  $v_f = 0.001044\text{ m}^3/\text{kg}$  and  $v_g = 1.67290\text{ m}^3/\text{kg}$

And  $v_f < v < v_g$ . Hence saturated state.

$$\text{Quality } x = \frac{(v - v_f)}{v_{fg}} = \frac{(0.00315 - 0.001044)}{1.67185} = 0.001255 \text{-----(1)}$$

Problem 2: Given: Piston-cylinder assembly with air.

State 1:  $P_1 = 100\text{ kPa}$

$$V_1 = 1\text{ L } (= 1 \cdot 10^{-3}\text{ m}^3)$$

$$T_1 = 300\text{ K}$$

State 2:  $V_2 = 2\text{ L } (= 2 \cdot 10^{-3}\text{ m}^3)$ ; Piston hits the stops

State 3:  $T_3 = 900\text{ K}$

Solution: The external pressure throughout the process is constant and is the sum of the atmospheric pressure and the pressure due to the piston's weight. During the process 1-2, there is free motion of the piston and hence the pressure of air is constant while the temperature and volume change. During the process 2-3 the stops restrict further motion of the piston. Hence the volume is constant and the temperature and pressure change.

Assumption: Air is a perfect gas

1-2 is a constant pressure process. Therefore,  $\frac{V_1}{T_1} = \frac{V_2}{T_2}$  or,  $T_2 = \frac{V_2 T_1}{V_1}$

$$\text{Hence } T_2 = \frac{(2 * 10^{-3})(300)}{(1 * 10^{-3})} = \mathbf{600 \text{ K}} \text{ -----(a)}$$

3-4 is a constant volume process. Therefore,  $\frac{P_2}{T_2} = \frac{P_3}{T_3}$  or,  $P_3 = \frac{P_2 T_3}{T_2}$

$$\text{Hence } P_3 = \frac{(100)(900)}{(600)} = \mathbf{150 \text{ kPa}} \text{ -----(b)}$$

Total work done is during the process is  $W_{1-3}$

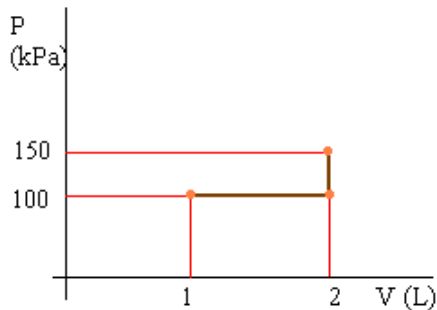
$$W_{1-3} = W_{1-2} + W_{2-3}$$

Since 2-3 is a constant volume process,  $dV_{2-3} = 0$ . Hence  $W_{2-3} = 0$

$$W_{1-3} = W_{1-2} = P_1 (V_2 - V_1) \text{ (1-2 is a constant pressure process)}$$

$$= (100)(2 * 10^{-3} - 1 * 10^{-3}) = \mathbf{0.1 \text{ kJ}} \text{ (work done by the system)-----(c)}$$

(d)



**Problem 3:** Given: Rigid, insulated tank divide by an un-insulated rigid divider, into two parts A and B, containing water.

State 1: Part A:  $m_{A1} = 0.1 \text{ kg}$

Part B:  $m_{B1} = 0.2 \text{ kg}$

$$T_{A1} = 200 \text{ }^\circ\text{C} (= 473.15 \text{ K})$$

$$T_{B1} = 80 \text{ }^\circ\text{C} (= 353.15 \text{ K})$$

$$P_{A1} = 100 \text{ kPa}$$

$$\text{quality } x_{B1} = 0.8$$

State 2:

$$T_{A2} = 150 \text{ }^\circ\text{C} (= 423.15 \text{ K})$$

$$T_{B2} = 90 \text{ }^\circ\text{C} (= 363.15 \text{ K})$$

$$P_{A2} = 50 \text{ kPa}$$

Heat transferred from A to B

Solution:

First law for the whole system,  $\Delta U = Q_{12} - W_{12}$

where  $Q_{12} = 0$  (insulated), and  $W_{12} = 0$  (rigid;  $dV = 0$ )

Hence the **First law for the whole system is**,  $\Delta U = 0$  or  $\Delta U_A + \Delta U_B = 0$ -----(a)

The divider between A and B being rigid,  $dV = 0$  and hence  $(W_{12})_A = 0$  and  $(W_{12})_B = 0$ . But is not insulated. Hence there is heat transfer. Also  $(Q_{12})_A = -(Q_{12})_B$

**First law for part A is**,  $\Delta U_A = (Q_{12})_A$  i.e.,  $U_{A2} - U_{A1} = (Q_{1-2})_A$ -----(a)

**First law for part B is**,  $\Delta U_B = (Q_{12})_B$  i.e.,  $U_{B2} - U_{B1} = (Q_{1-2})_B = U_{A1} - U_{A2}$  -----(a)

From first law for A,  $U_{A2} - U_{A1} = (Q_{1-2})_A = m_A(u_{A2} - u_{A1})$

Tables for wates show that A in states 1 and 2 is in superheated state. Hence from Table B.1.3, we get  $u_{A1} = 2658.05$  kJ/kg and  $u_{A2} = 2585.61$  kJ/kg.

Hence  $(Q_{1-2})_A = m_A(u_{A2} - u_{A1}) = (0.1)(2585.61 - 2658.01) = -7.244$  kJ (heat removed from A) --(b)

From table B.1.1, at  $T_{B1} = 80$  °C and quality  $x_{B1} = 0.8$ ,  $u_f = 334.84$  kJ/kg and  $u_{fg} = 2147.36$  kJ/kg.

Therefore,  $u_{B1} = u_f + x_{B1} u_{fg} = 334.84 + 0.8 * 2147.36 = 2052.728$  kJ/kg

$$(Q_{1-2})_B = -(Q_{1-2})_A = U_{B2} - U_{B1} = 7.244 \text{ kJ}$$

$$\text{Hence } u_{B2} = \frac{(Q_{1-2})_B}{m_B} + u_{B1} = \frac{7.244}{0.2} + 2052.728 = 2088.948 \text{ kJ/kg}$$

From Table B.1.1 at  $T_{B2} = 90$  °C,  $u_f = 376.82$  kJ/kg,  $u_g = 2494.52$  and  $u_{fg} = 2117.70$  kJ/kg

Since  $u_f < u_{B2} < u_g$ , it is in saturated state.

$$\text{The quality } x_{B2} = \frac{(u_{B2} - u_f)}{u_{fg}} = \frac{(2088.948 - 376.82)}{2117.70} = 0.8085 \text{-----(c)}$$