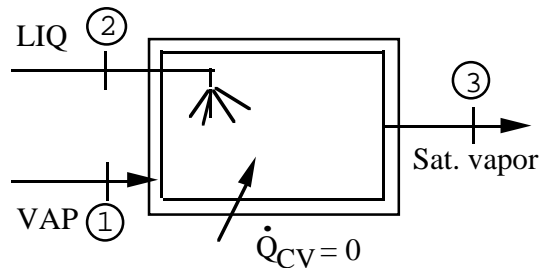


ME 24-221
Thermodynamics I

Solution to Assignment No: 6
Due Date: 20 October 2000
Fall 2000
Instructor: J.Murthy

Pb# 6.8

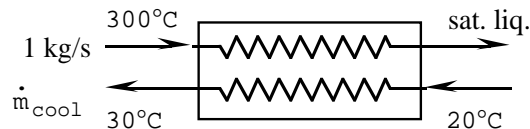


$$\text{Cont.: } \dot{m}_1 + \dot{m}_2 = \dot{m}_3$$

Energy Eq.:

$$\begin{aligned} \dot{m}_1 h_1 + \dot{m}_2 h_2 &= \dot{m}_3 h_3 \\ 0.5 \times 3195.7 + \dot{m}_2 \times 171.97 &= (0.5 + \dot{m}_2) 2797.9 \\ \Rightarrow \dot{m}_2 &= \mathbf{0.0757 \text{ kg/s}} \end{aligned}$$

Pb#6.14



C.V. Heat exchanger

$$\begin{aligned} \dot{m}_{\text{cool}} h_{20} + \dot{m}_{\text{H}_2\text{O}} h_{300} &= \\ \dot{m}_{\text{cool}} h_{30} + \dot{m}_{\text{H}_2\text{O}} h_{f, 10\text{kPa}} & \end{aligned}$$

Table B.1.1: $h_{20} = 83.96 \text{ kJ/kg}$, $h_{30} = 125.79 \text{ kJ/kg}$

Table B.1.3: $h_{300, 10\text{kPa}} = 3076.5 \text{ kJ/kg}$, B.1.2: $h_{f, 10\text{kPa}} = 191.83 \text{ kJ/kg}$

$$\dot{m}_{\text{cool}} = \dot{m}_{\text{H}_2\text{O}} \frac{h_{300} - h_{f, 10\text{kPa}}}{h_{30} - h_{20}} = 1 \times \frac{3076.5 - 191.83}{125.79 - 83.96} = \mathbf{69 \text{ kg/s}}$$

Pb# 6.20

$$\dot{m}_i = A_i \mathbf{V}_i / v_i = \dot{m}_e = A_e \mathbf{V}_e / v_e, \quad h_i + (1/2) \mathbf{V}_i^2 = h_e + (1/2) \mathbf{V}_e^2$$

$$h_e - h_i = (1/2) \times 200^2 / 1000 - (1/2) \times 20^2 / 1000 = 19.8 \text{ kJ/kg}$$

$$T_e = T_i + 19.8 / 1.35 = \mathbf{319.73 \text{ K}}$$

$$v_e = v_i (A_e \mathbf{V}_e / A_i \mathbf{V}_i) = (RT_i / P_i) (A_e \mathbf{V}_e / A_i \mathbf{V}_i) = RT_e / P_e$$

$$P_e = P_i (T_e / T_i) (A_i \mathbf{V}_i / A_e \mathbf{V}_e)$$

$$= 100(319.73/300) (100 \times 200) / (860 \times 20) = \mathbf{123.93 \text{ kPa}}$$

Pb# 6.23

C.V. Throttle. SSSF, Process with: $q = w = 0$;

Energy Eq.: $h_i = h_e$, Ideal gas $\Rightarrow T_i = T_e = 20^\circ\text{C}$

$$\dot{m} = \frac{A\mathbf{V}}{RT/P} \quad \text{But } \dot{m}, \mathbf{V}, T \text{ are constant } \Rightarrow P_i A_i = P_e A_e$$

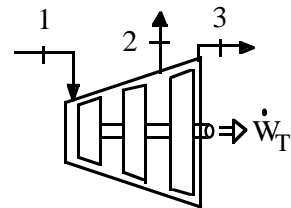
$$\Rightarrow \frac{D_e}{D_i} = \left(\frac{P_i}{P_e}\right)^{1/2} = \left(\frac{1.2}{0.1}\right)^{1/2} = \mathbf{3.464}$$

Pb# 6.29

C.V. Turbine SSSF, 1 inlet and 2 exit flows.

Table B.1.3 $h_1 = 3582.3 \text{ kJ/kg}$, $h_2 = 3137 \text{ kJ/kg}$

Table B.1.2 : $h_3 = h_f + x_3 h_{fg} = 384.3 + 0.95 \times 2278.6$
 $= 2549.1 \text{ kJ/kg}$



$$\text{Cont.: } \dot{m}_1 = \dot{m}_2 + \dot{m}_3 ; \quad \text{Energy: } \dot{m}_1 h_1 = \dot{W}_T + \dot{m}_2 h_2 + \dot{m}_3 h_3$$

$$\dot{m}_3 = \dot{m}_1 - \dot{m}_2 = 80 \text{ kg/s} , \quad \dot{W}_T = \dot{m}_1 h_1 - \dot{m}_2 h_2 - \dot{m}_3 h_3 = \mathbf{91.565 \text{ MW}}$$

Pb# 6.36

C.V. Compressor, SSSF energy Eq.: $q + h_i + \mathbf{V}_i^2/2 = h_e + \mathbf{V}_e^2/2 + w$

Here $q \cong 0$ and $\mathbf{V}_i \cong 0$ so for const C_{P0}

$$-w = C_{P0}(T_e - T_i) + \mathbf{V}_e^2/2 = 1.004(430 - 20) + \frac{(90)^2}{2 \times 1000} = 415.5 \text{ kJ/kg}$$

$$\dot{m} = \frac{5000}{415.5} = \mathbf{12.0 \text{ kg/s}}$$